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Membranes in salinity gradient power generation

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Outline

» Salinity gradient power (SGP)

- Concept and some figures

» Overview of technologies

■ Pressure Retarded Osmosis (PRO)

- ✓ Current status and developments
- ✓ Market Players
- ✓ Challenges

■ Reverse Electrodialysis (RED)

- ✓ Current status and developments
- ✓ Market Players
- ✓ Challenges

Salinity gradient power (SGP) – concept

Gibbs free energy of mixing low concentration (LC) and high concentration (HC) streams, ΔG_{mix} :

$$-\frac{\Delta G_{\text{mix}, V_{\text{LC}}^0}}{\nu RT} \approx \frac{c_{\text{M}}}{\phi} \ln c_{\text{M}} - c_{\text{LC}} \ln c_{\text{LC}} - \frac{1-\phi}{\phi} c_{\text{HC}} \ln c_{\text{HC}}$$

C molar concentration

ϕ volume fraction of low concentration (LC) stream

ν number of electrolyte ions (e.g., 2 for NaCl)

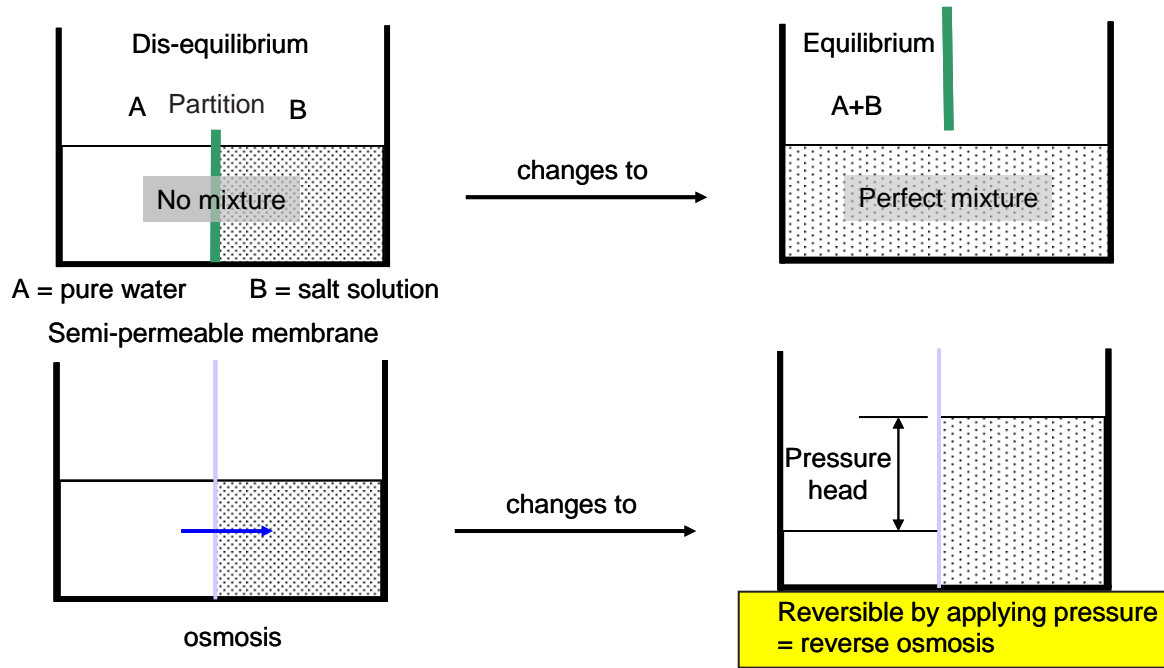
R gas constant

T absolute temperature

Subscripts:

M – mixture; LC – low conc stream; HC – high conc stream

Salinity gradient power (SGP) - concept



- seawater (35 kg of salt per m³): osmotic pressure = 2,700,000 Pa => 27 bar => **270 m of water column**
- to squeeze potable water out of seawater, a pressure of over 27 bar must be applied

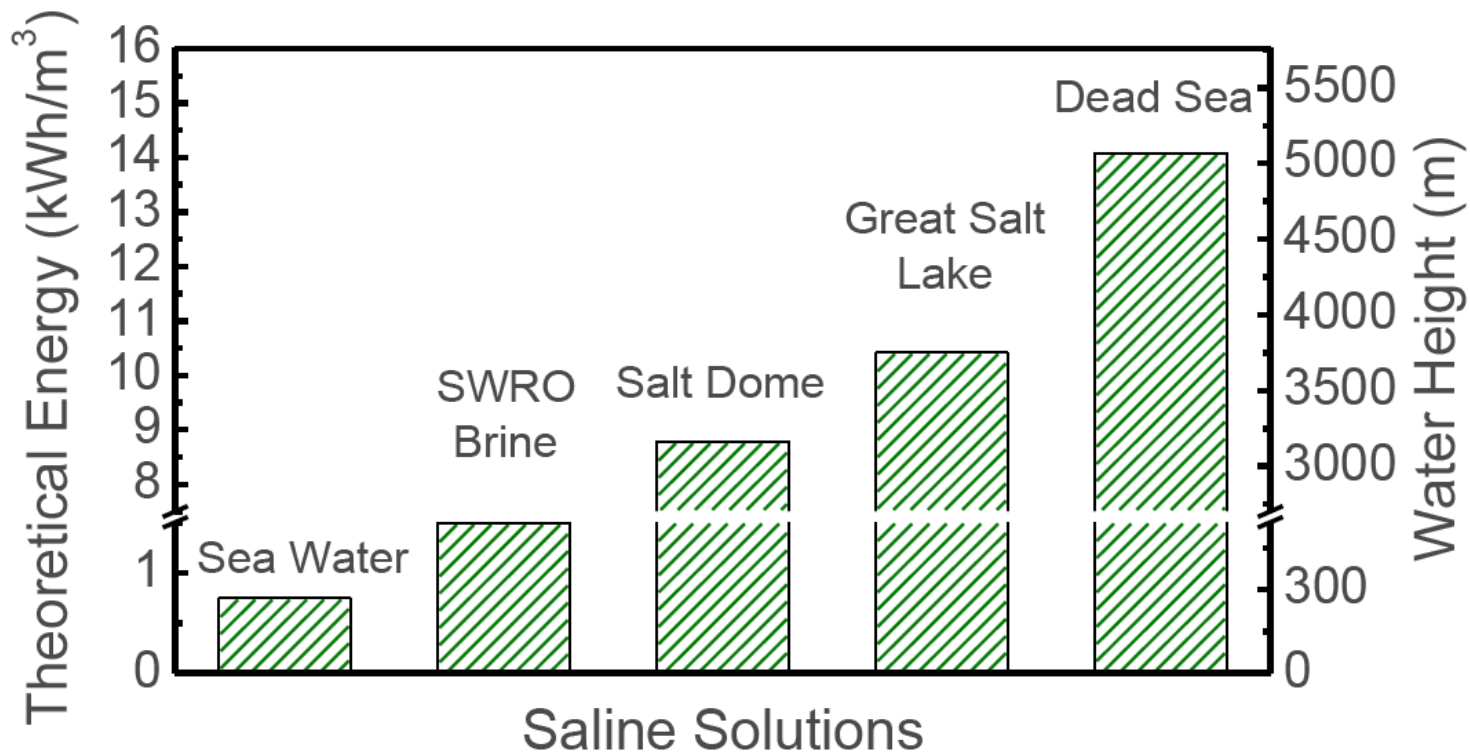
Salinity gradient power (SGP) – some figures

» Indirect calculation: seawater osmotic energy content:

$$E = P \times V = P \times S \times d$$

- ✓ producing one m³ fresh water from an infinite amount of seawater :
 $E = 2,700,000 \text{ N/m}^2 \times 1 \text{ m}^2 \times 1 \text{ m} = 2,700,000 \text{ Nm} = \mathbf{2,7 \text{ MJ}}$
- ✓ seawater : $2.7 \text{ MJ/m}^3 = 0.75 \text{ kWh/m}^3$
- ✓ equals the potential energy “m x g x h” of 1 m³ of water (1000 kg) at a height of about 270 m
- ✓ in theory: the osmotic energy within 1 m³ of seawater allows to lift 1 m³ of water to a height of 270 m

Energy of mixing from natural salinity gradient



For river water–seawater mixing: $\Delta G_{\text{mix}} \sim 0.8 \text{ kWh/m}^3$

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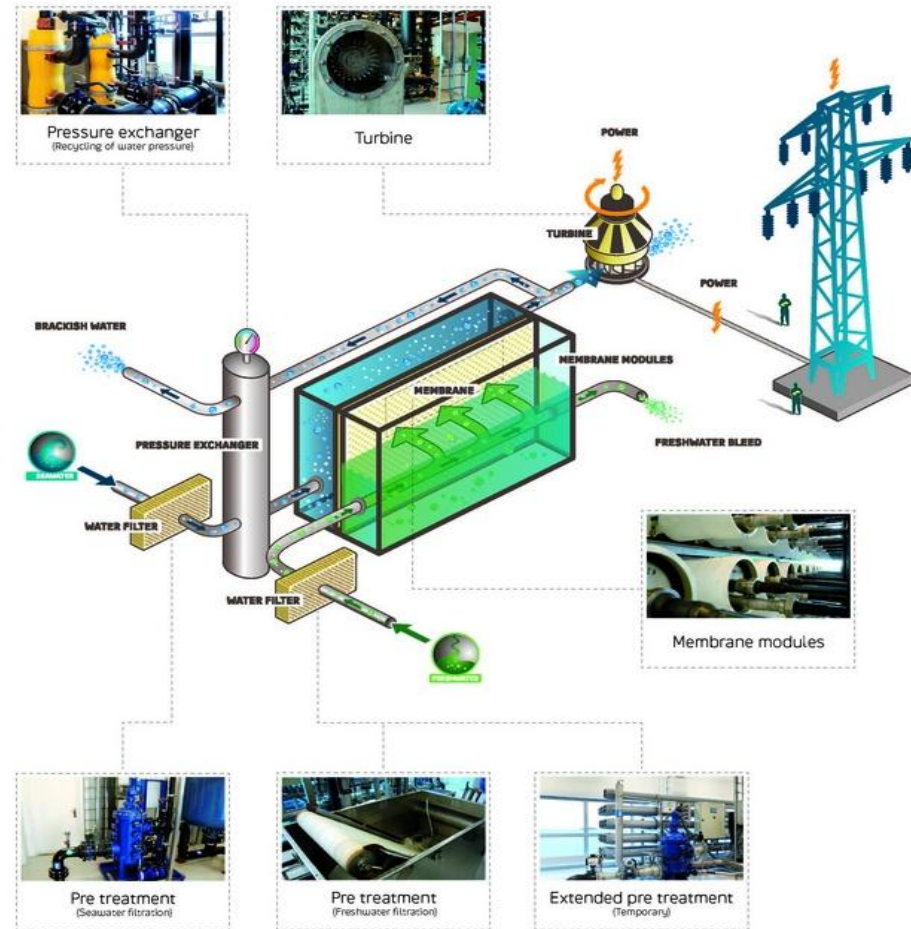
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■ Reverse Electrodialysis (RED)

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SGP-PRO (Pressure retarded osmosis)

- » Most intensely studied and advanced SGP principle: research initiated by Sydney Loeb (1976)
- » Principle of operation:
 - Transport of water through membrane from low concentration to high concentration
 - Skin layer in contact with high salinity side
 - Back pressure on high salinity side and increase of volume



SGP-PRO (Pressure retarded osmosis)

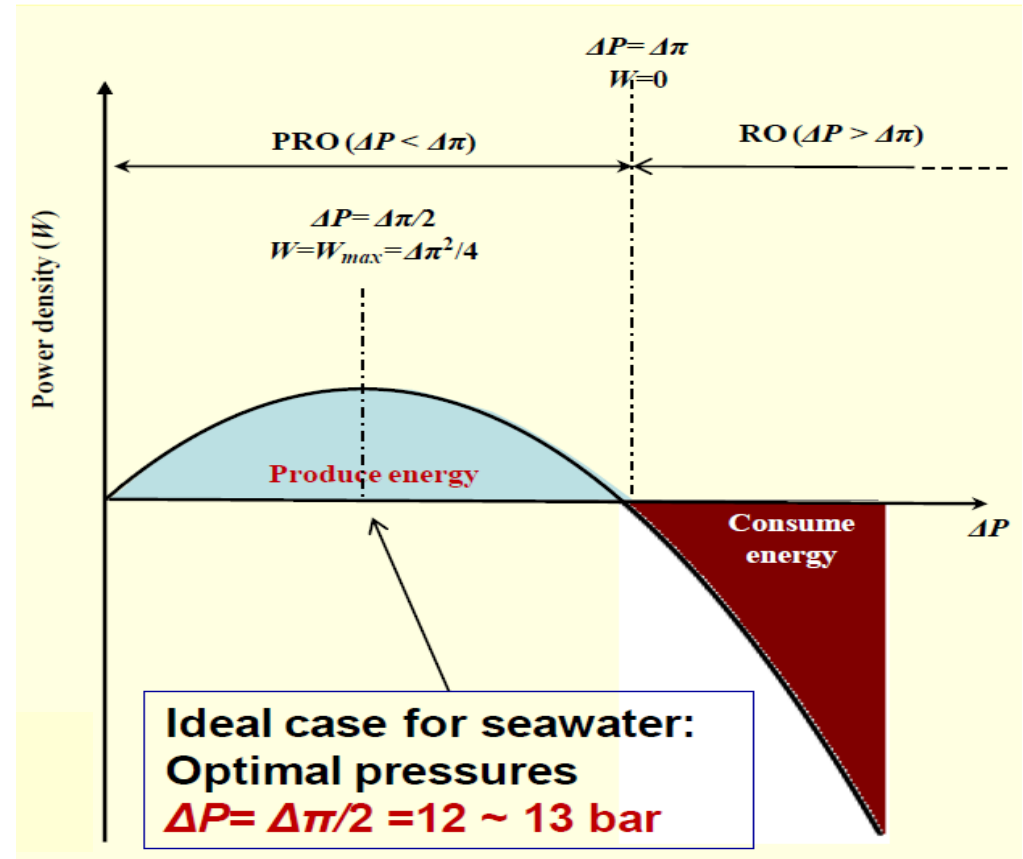
» RO versus PRO

- » $\Delta p = 0 \rightarrow \text{FO}$
- » $0 < \Delta p < \Delta \pi \rightarrow \text{PRO}$
- » $\Delta p > \Delta \pi \rightarrow \text{RO}$

» Work delivered by transport of water through membrane

$$W = A \cdot (\Delta \pi - \Delta p) \cdot \Delta p$$

$$W_{MAX} = \frac{\Delta \pi^2}{4}$$



SGP-PRO (Pressure retarded osmosis)

» Membrane challenges

□ Rejection layer:

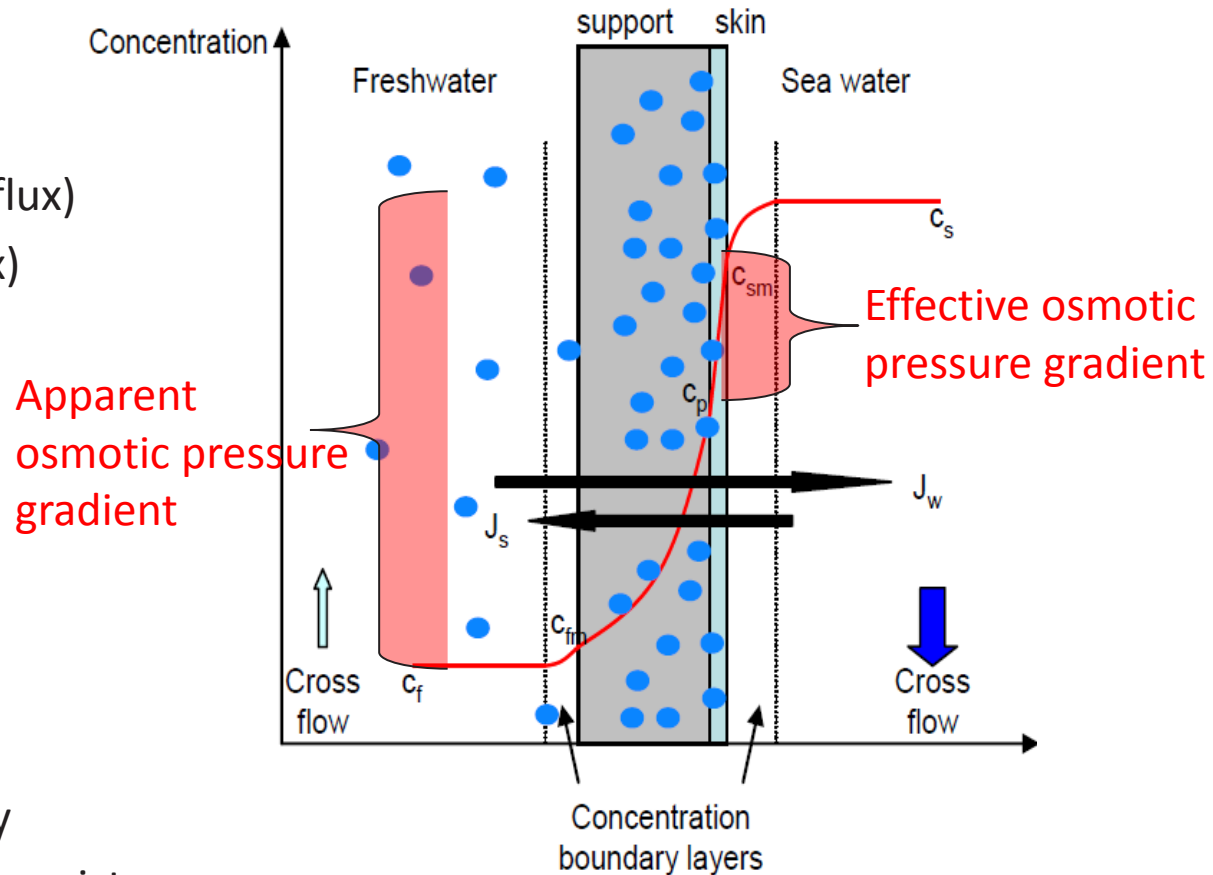
- High A-value (water flux)
- Low B-value (salt flux)

□ Support layer:

- Small S-value

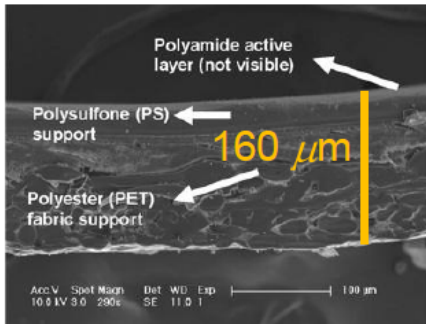
$$\lambda = \frac{\varepsilon}{\tau \times Q^{1/2}}$$

- Thinner
- More porous
- Lower tortuosity
- Higher back-pressure resistance



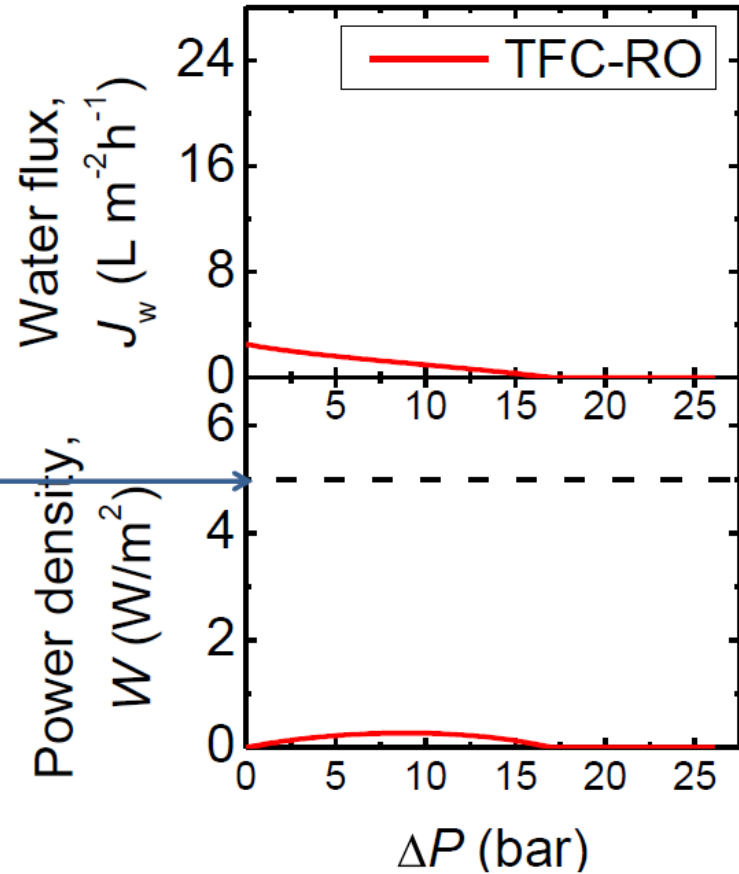
RO Membranes Perform Poorly in PRO

Commercial RO polyamide thin-film composite membrane



Target:
5 W/m²

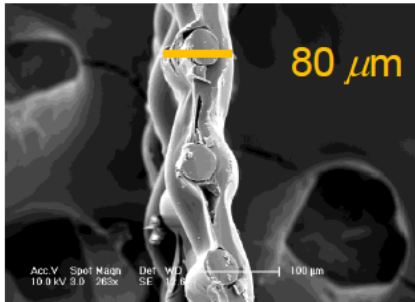
Skillhagen *Desal. & Water Treatment* **2010**, 15 (1-3), 271-278



Draw: Seawater
Feed: River water

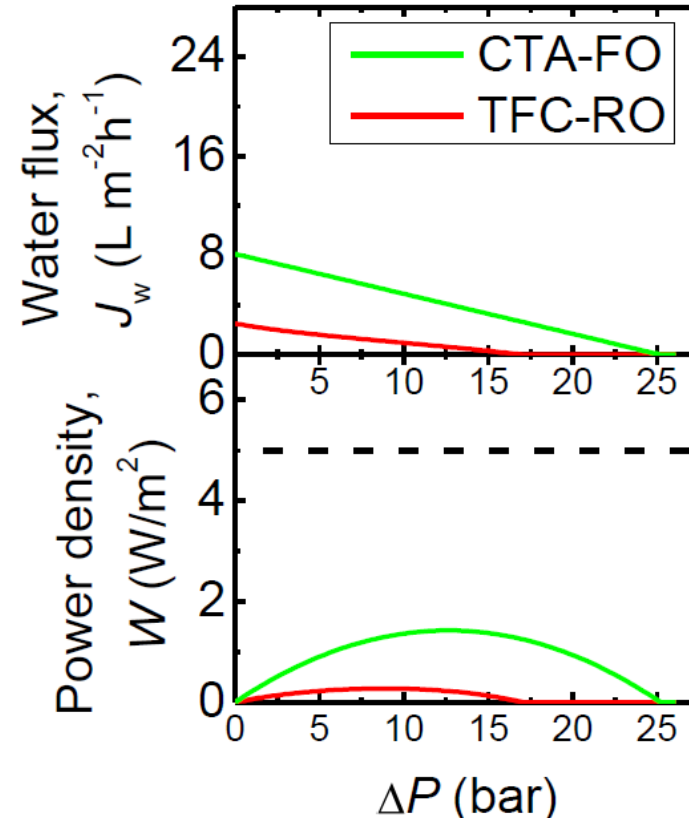
Commercial Cellulose Acetate FO Membrane has Limitations

Commercial FO cellulose triacetate asymmetric membrane



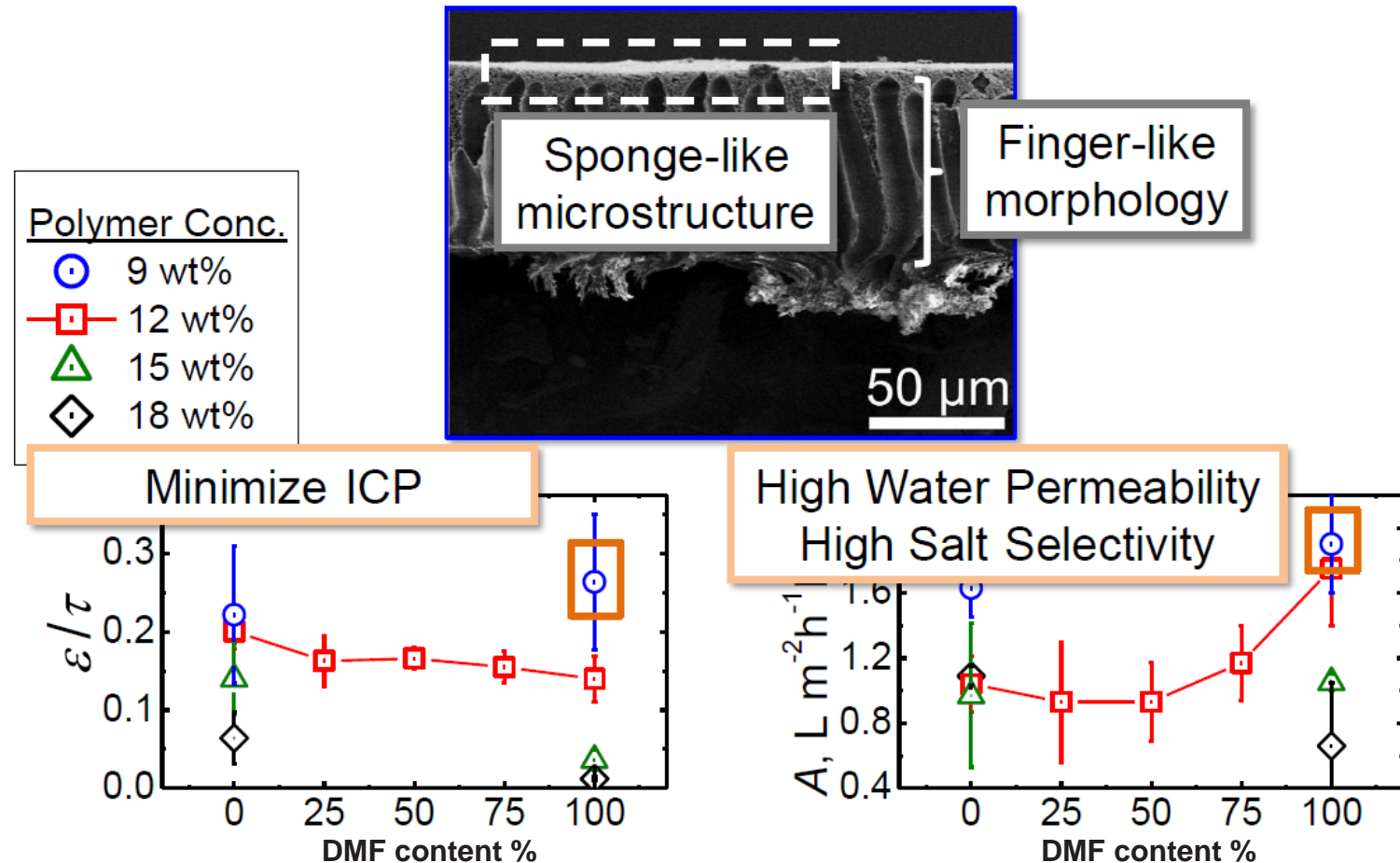
Limitations

- Low intrinsic water permeability
- Low salt rejection
- Narrow operable pH range



Draw: Seawater
Feed: River water

Performance Determined by Active and Support Layer Properties

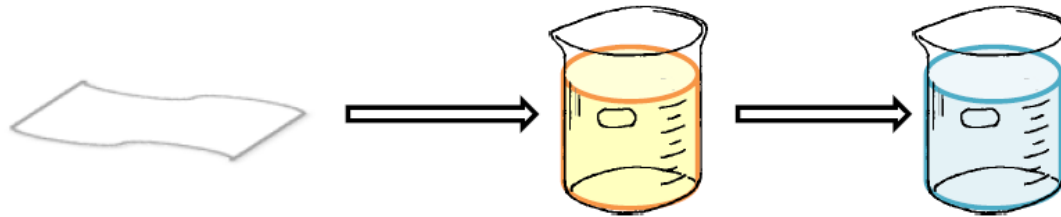


Tiraferri et al. *J. Membr. Sci.* **2011**, 367, 340-352

PSf /NMP-DMF phase-inversion process

Increase Membrane Permeability on the Expense of Membrane Selectivity

- Post-treatment of polyamide selective layer

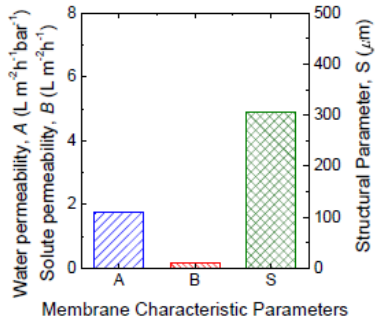


Membrane	Chlorine	Alkaline	Δ permeability
“LP” Low permeability	No post-treatment		–
“MP” Medium permeability	1,000 ppm NaOCl @ pH 7.0, 60 mins	0.1 M NaOH, 16 h	↑
“HP” High permeability	2,000 ppm NaOCl @ pH 7.0, 120 mins	0.1 M NaOH, 62 h	↑↑

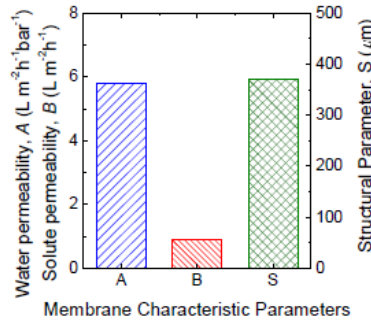
Yip et al. *Environ. Sci. Technol.* **2011**, 45, 4360–4369

TFC-PRO Membrane Performance

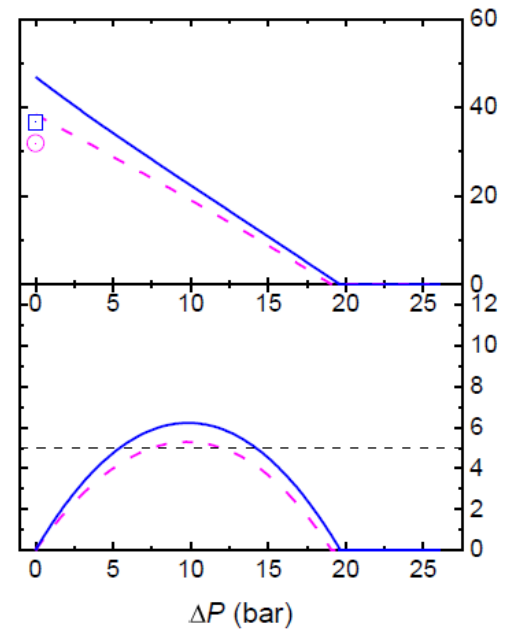
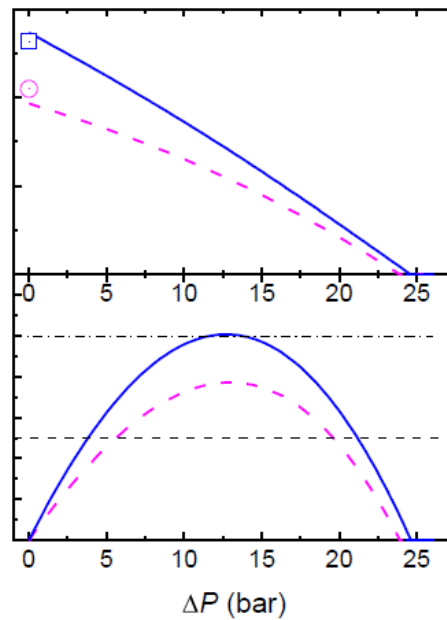
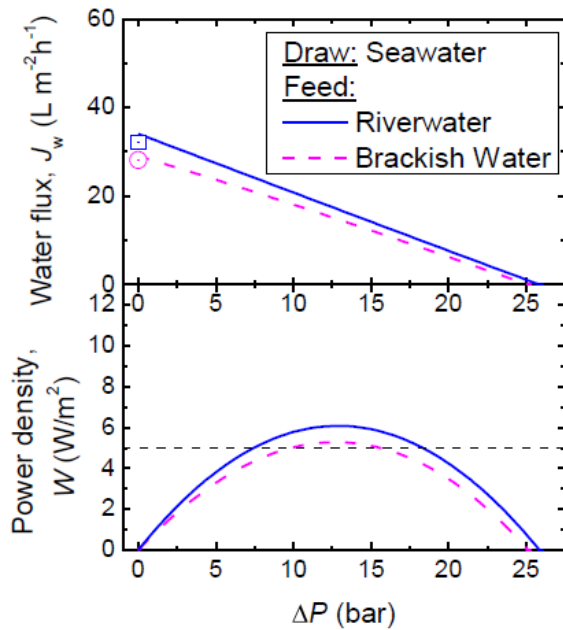
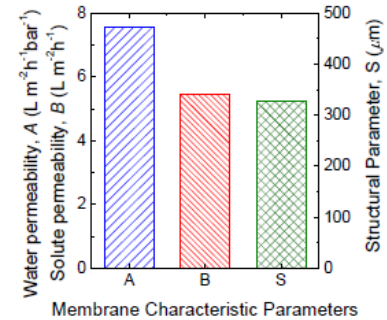
LP



MP



HP



SGP-PRO Market Players

- HTI: supplier CTA FO membrane (first generation)

OsMEM™ FO Cellulose Triacetate Flat Sheet Membrane

- Commercial 40 inch production
- Woven and non-woven backed versions
- Spiral FO modules (2.5", 4" and 8" diameter by 40" lengths, single element and multi-element configuration)
- Plate and frame cassette modules
- Available for large production orders

HTI's historical and founding membrane product. Extremely hydrophilic and oleophobic (contact angle 60°). Excellent non-fouling properties. Long lived and Chlorine tolerant.

- Average flux in FO mode - 9.0 LMH (1M NaCl vs DI water)
- NaCl rejection - 99% (<500 mg/ liter)
- Operating pH range - 3 to 8



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SGP-PRO Market Players

□ HTI: supplier TFC FO membrane (novel product)

Announcing Commercial Availability of OsMEM™ FO TFC Flat Sheet Membrane Modules

- High performance thin film composite (TFC) polymer membrane
- 40 inch production on durable woven backing - very robust
- Spiral FO modules (2.5", 4" and 8" diameter by 40" length, single and multi-module configuration)
- Available for large production orders

HTI's high performance FO membrane product is hydrophilic (contact angle 45°). Excellent non-fouling properties.

- Average flux in FO mode - min 20 LMH (1M NaCl vs DI water)
- NaCl rejection - 99.4 % (<300mg/L salt leakage)
- PRO rating (flat cell - 160psi, 10 C) - 3.5 Watts/M²
- Operating pH range - 2 to 11



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SGP-PRO Market Players

❑ **Perifera Inc.: new membrane supplier FO**

- New FO membranes ready for commercial production (June 2012)
- TFC membranes → stable in wide range of pH & solvent, low propensity to foul
- High power density ~ 10-12 W/m²

❑ **Pilot- / Demo-projects**

- Norway: Statkraft project (Statkraft + Hydranautics / Nitto Denko)
- Japan: Mega-ton Water System project (Toray)

Statkraft project

MAIN EXPERIENCES

- > No environmental showstoppers detected
- > Increased belief in commercial possibility
- > Possible to operate throughout seasonal variations
- > PRO membranes behave different in real conditions than in the lab
- > NOM fouling on FW side, main fouling issue

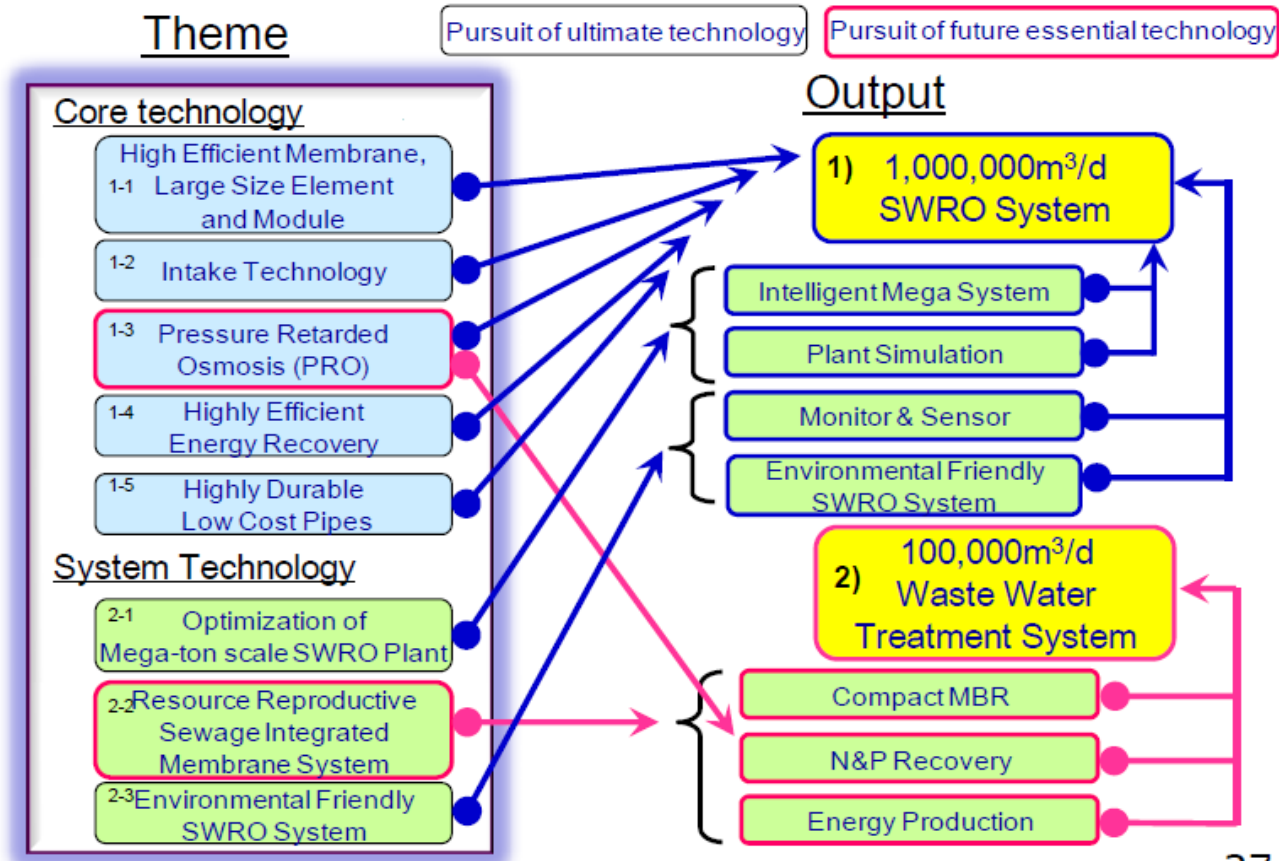


- “Proof of concept”
- System scale-up
- “Moving down the learning curve...”
- Membrane and component testing and optimisation
- Operation and maintenance experience
- Meeting place for manufactures and utilities

Mega-ton Water System

FIRST Program: Mega-ton Water System

Research Promotion Organization



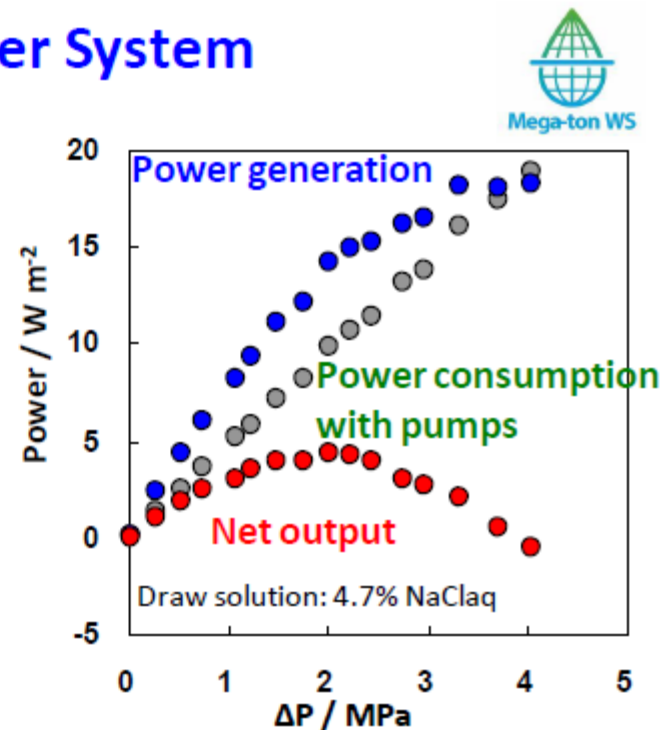
Mega-ton Water System

FIRST Program: Mega-ton Water System

Topics

Pressure Retarded Osmosis

- Hollow fibre membrane for power generation by PRO using seawater brine was newly developed.
- Net output was estimated at 4.4 W/m² when 4.7% of NaCl_{aq} was used, 9 W/m² is promising at 7% of seawater brine.
- Energy recovery for seawater desalination process was optimized by detailed PRO simulations.



PRO output corresponding to operation pressure

SGP-PRO

» Main challenges for the coming years

- High performance membranes
- Develop low-cost pretreatment
- Fouling issues
- Module design (spiral wound/HF)
- Upscaling (membrane production and PRO-systems)

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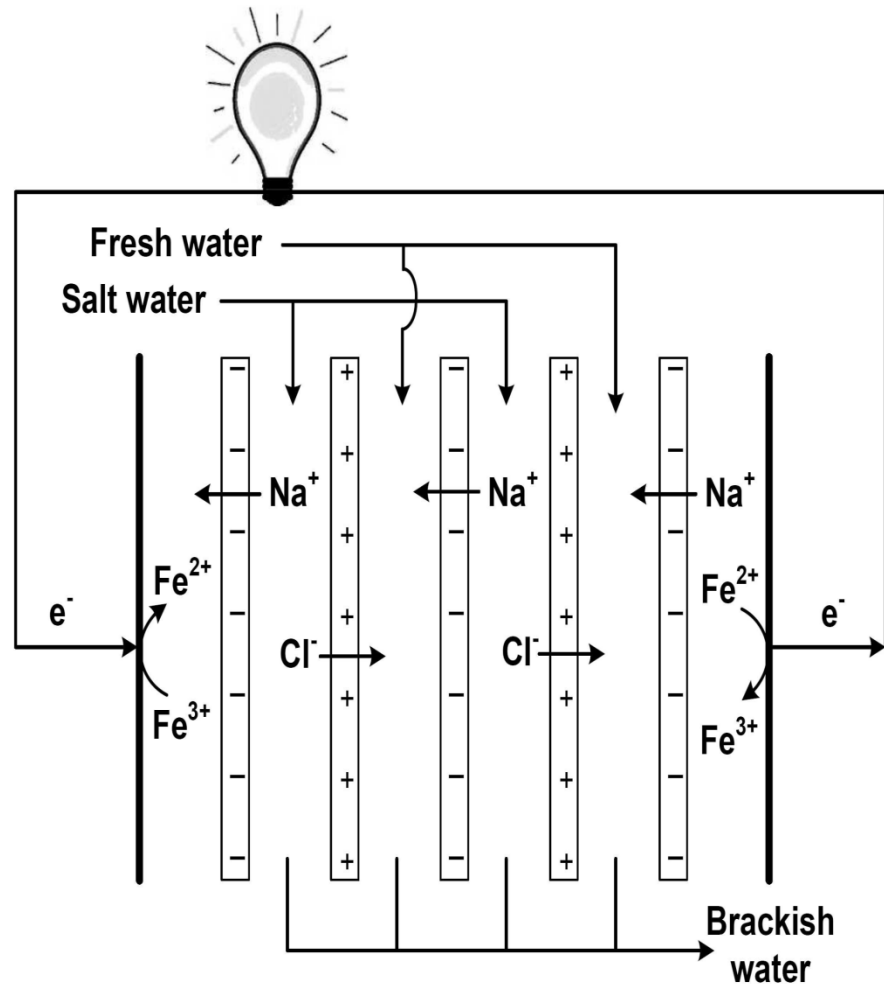
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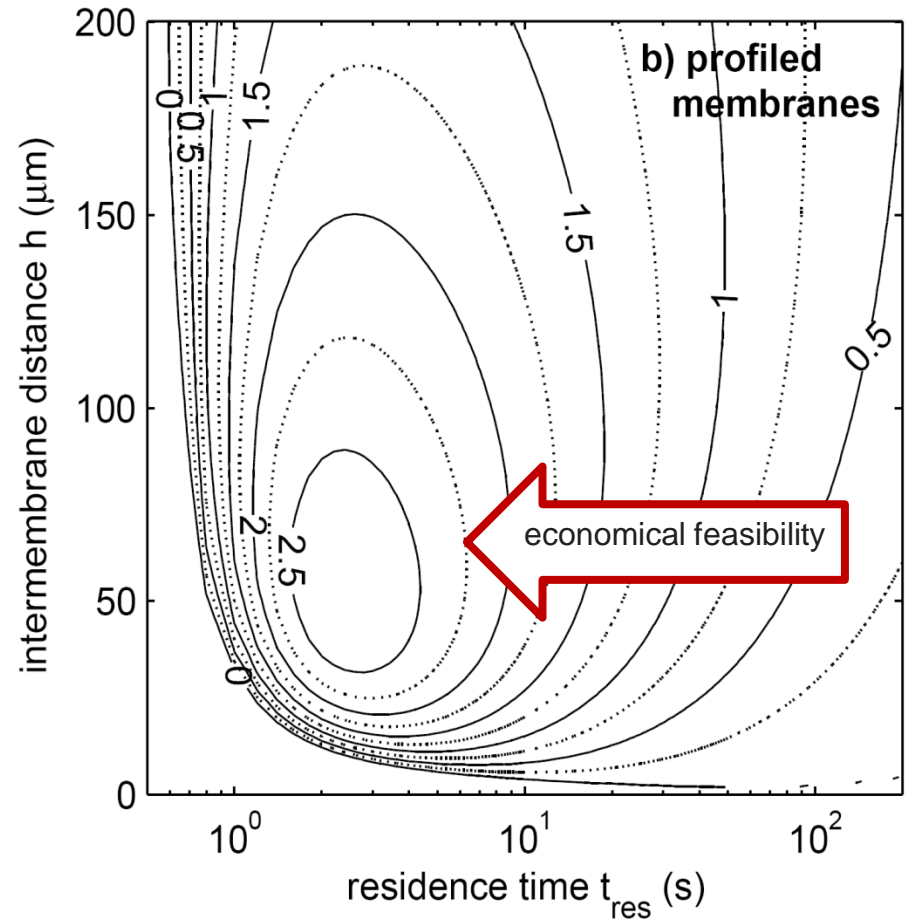
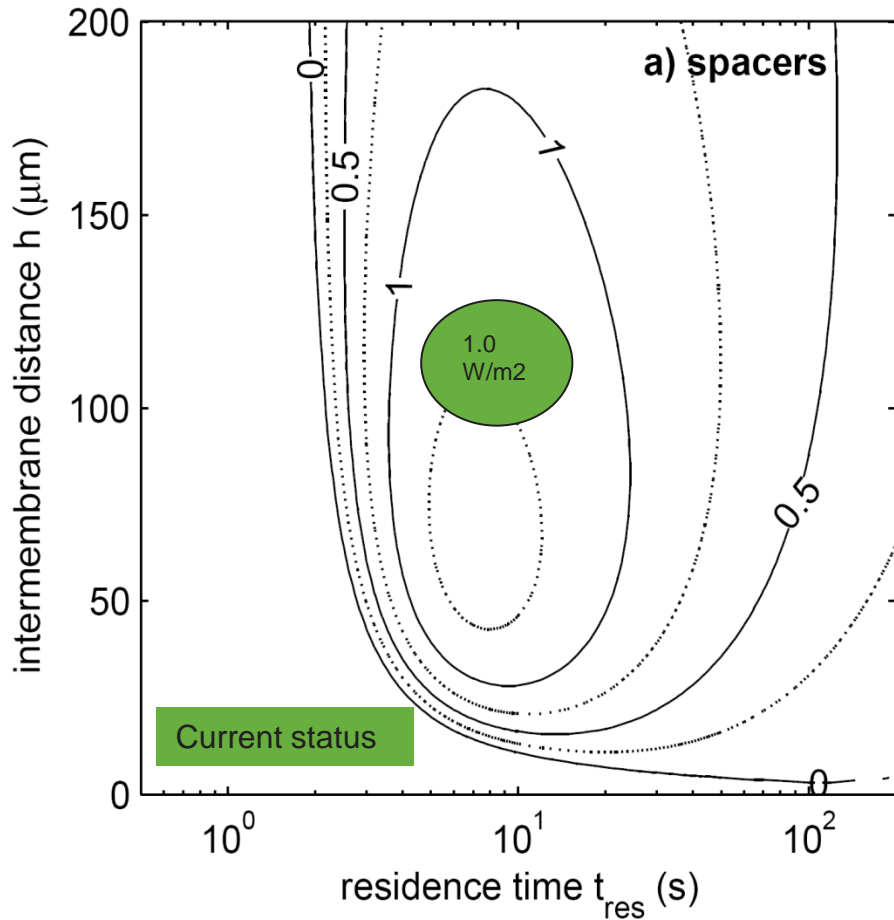
- ✓ Current status and developments
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SGP-RE (Reverse Electrodialysis)

- » Principle of operation:
 - » Ions are transported through membrane due to concentration gradient
 - » Cell potential is generated by selective diffusion of ions
 - » Electrode reactions induce electric current
 - » Applicable at different salinity gradients
 1. river – sea water
 2. brine – sea water

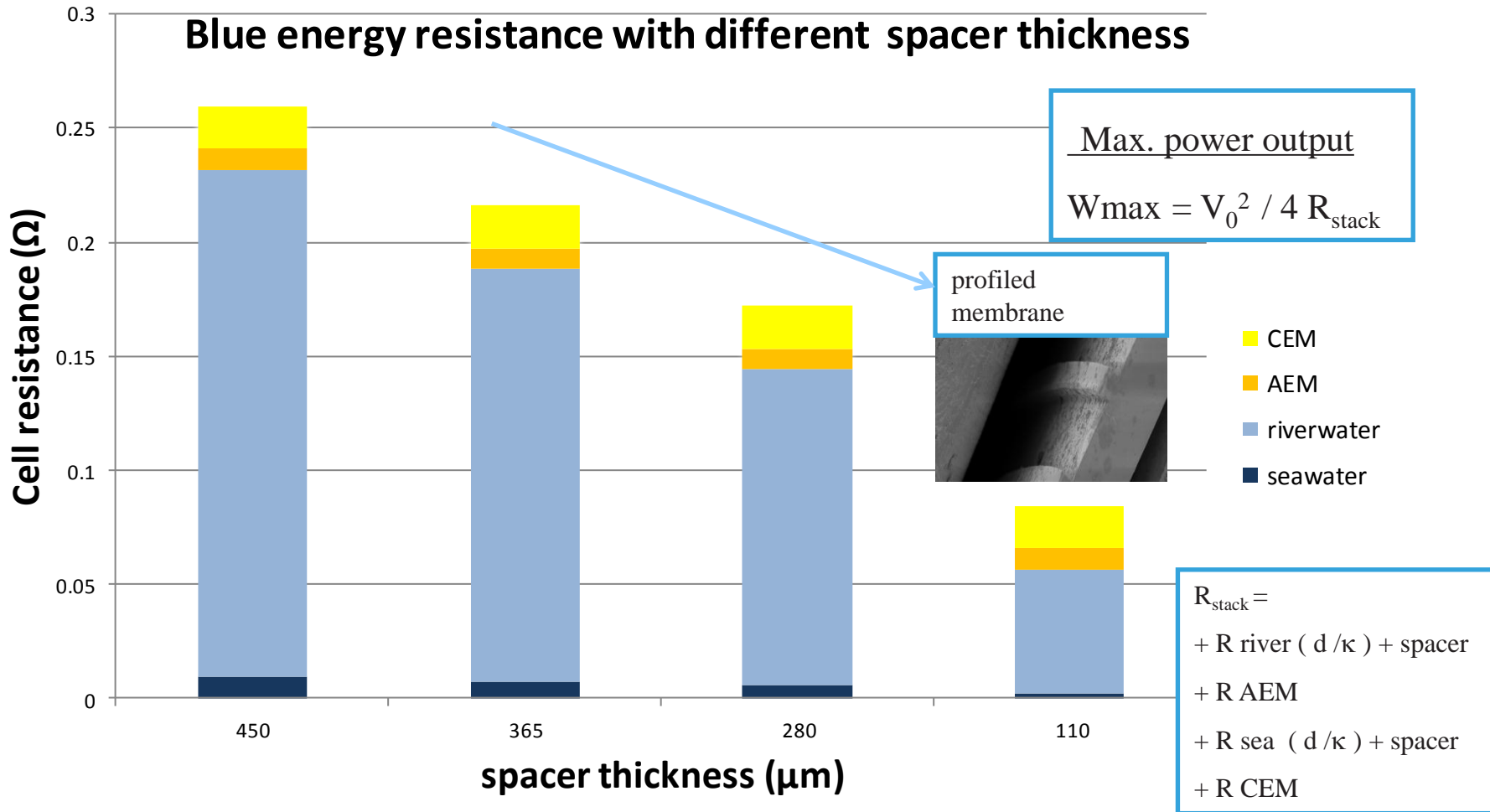


SGP-RE: Blue Energy (river-sea) status



Vermaas et al./ Energy Procedia (2011)

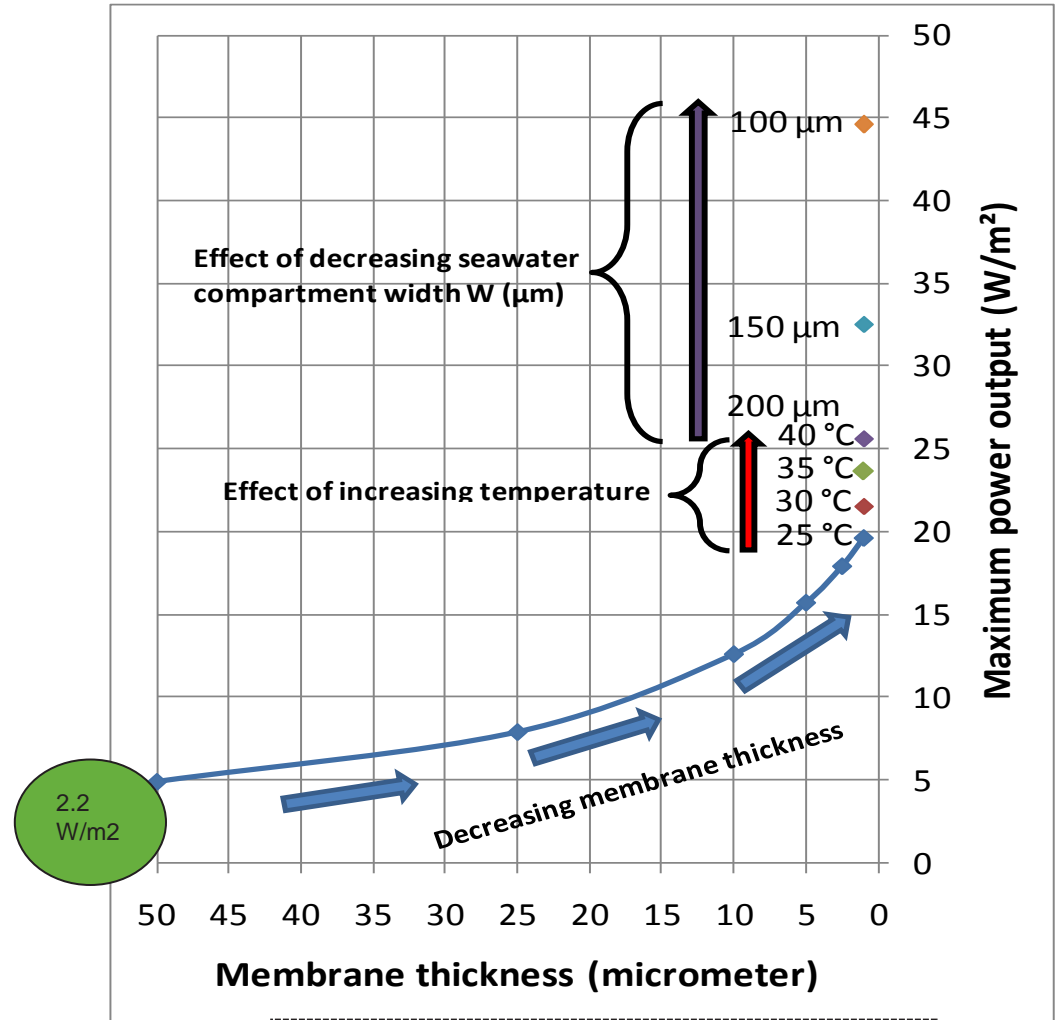
SGP-RE: Blue Energy (river-sea) development



SGP-RE: REAPower (brine – sea) status

- » REAPpower status
 - » 0.5 - 4.0 m NaCl
 - » FUJI R1 membranes
 - 120 micron thick
 - homogeneous
 - » 300 micron spacer

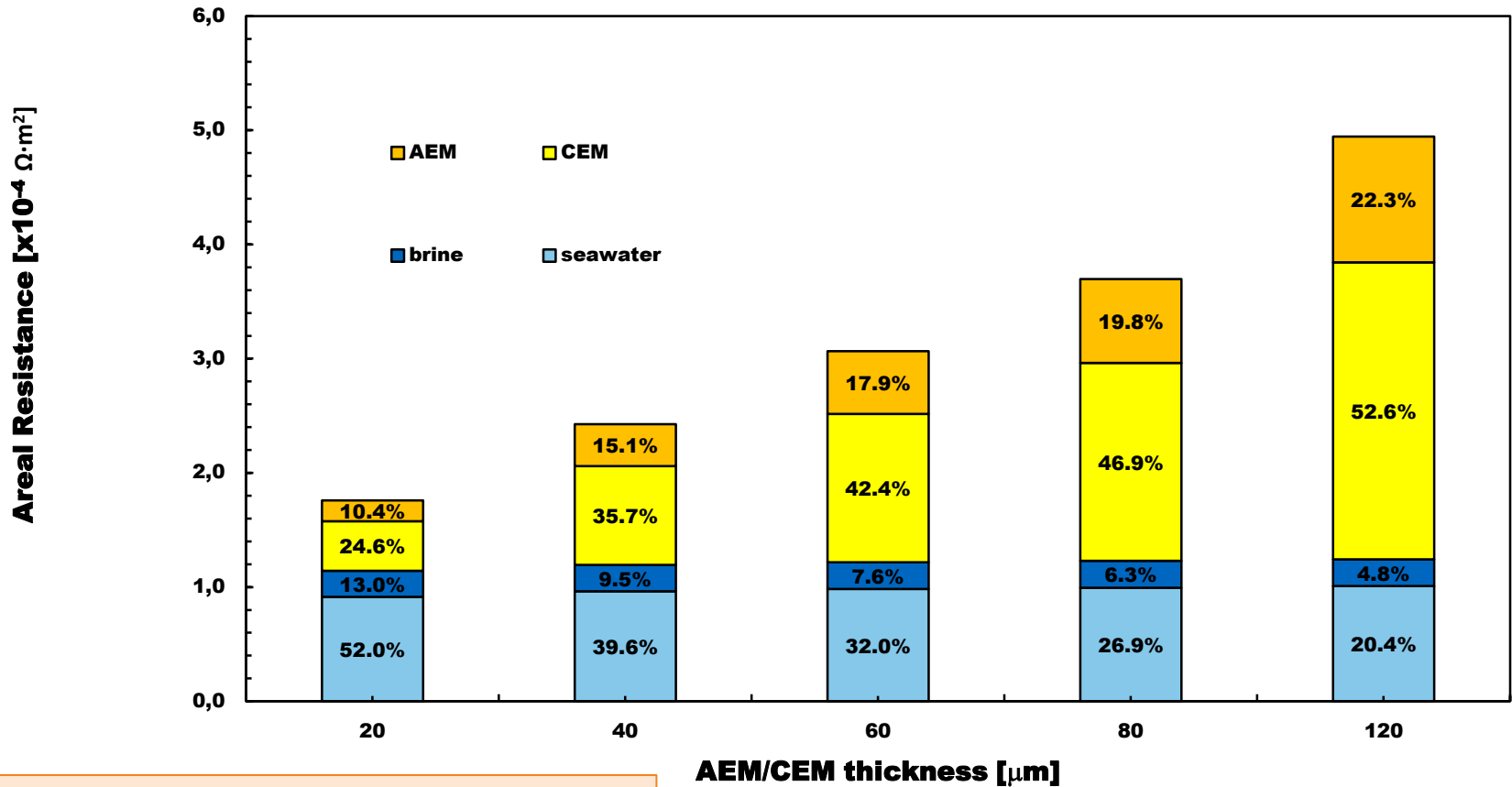
- » Highest value:
 - 2.2 W/m² cell pair



E. Brauns, Desalination 237 (2009) 378–391

SGP-RE: REAPower (brine – sea) development

development towards thinner membranes



Influence of IEMs thickness on resistance of the system.

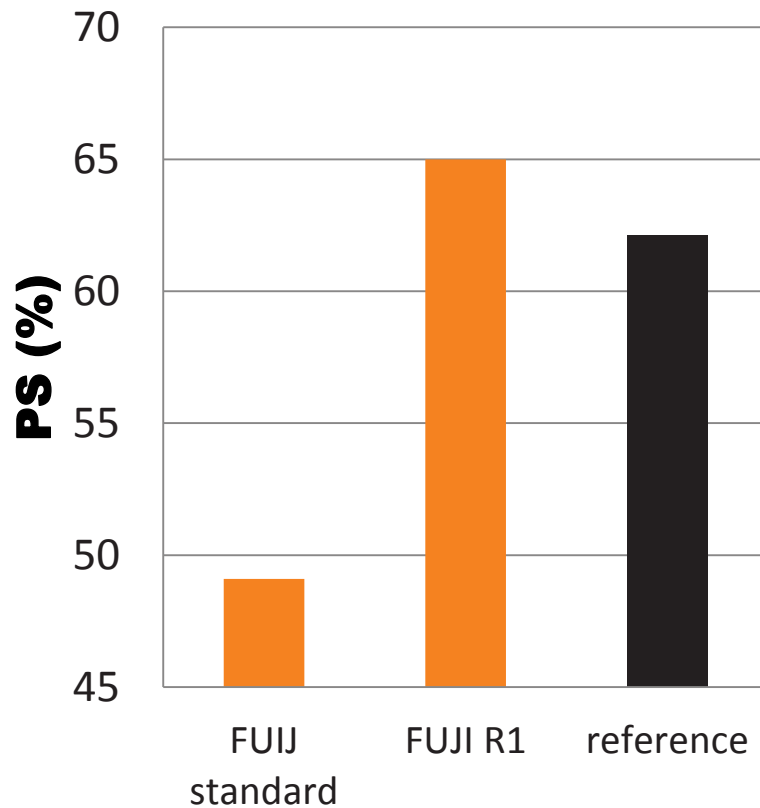
- Simulation of a 1000 cells stack assuming a linear decreasing of IEMs resistance with IEMs thickness.
- $\alpha_{AEM} = 0.65$, $\alpha_{CEM} = 0.90$.
- spacer thickness of seawater/brine compartments $d = 200$ micron.

Source: A multi-scale model for the Reverse ElectroDialysis process with seawater and concentrated brines by M. Tedesco University Palermo

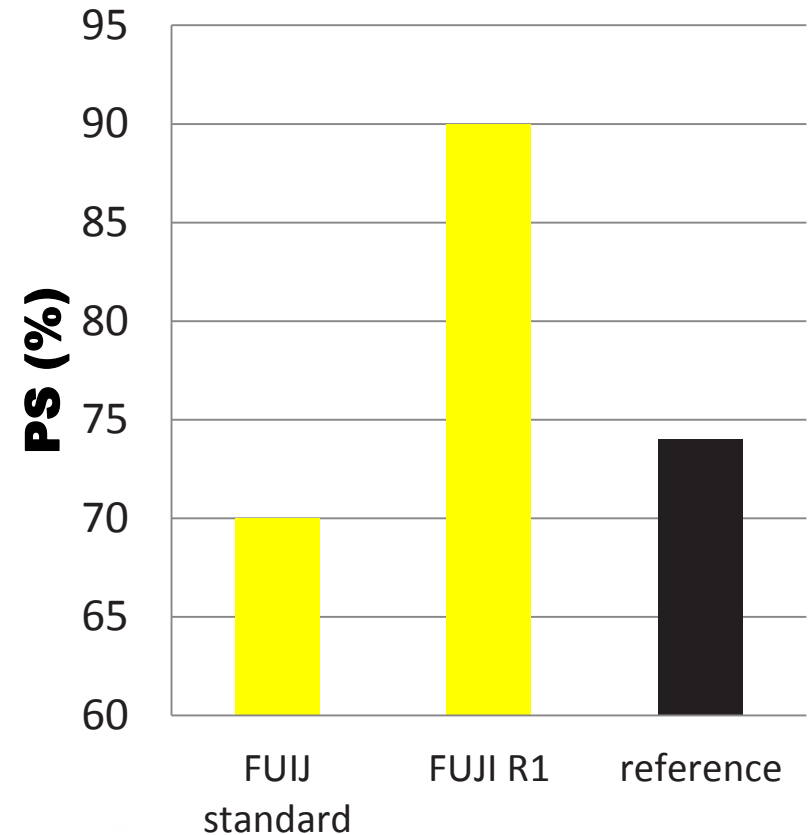
SGP-RE: REAPower (brine – sea) development

development high PS membranes at high salt concentration

AEM Permselectivity 0.5 – 4M NaCl



CEM Permselectivity 0.5 – 4 M NaCl



SGP-RE: Membrane market players

□ Main players

□ FUJI FILM

- cost competitive membranes
- commercially available (max. width 50 cm)

□ Kraton (only CEM), Fumatech



□ Increasing interest other IEM manufacturers

SGP-RE: main challenges coming years

» Blue Energy

- » river – sea water
- powerdensity increase $> 2 \text{ W/m}^2$
- reduce river channel resistance

» REAPower

- » brine – sea water
- powerdensity increase to $4\text{-}5 \text{ W/m}^2$
- reduce membrane resistance

- feed pre-filtration at low cost
- fouling
- scaling
- prove technology
- scale up to fieldtest pilots

SGP-RE: Blue Energy pilot Afsluitdijk

RED STACK

FUJIFILM

wetsus

brak water afv

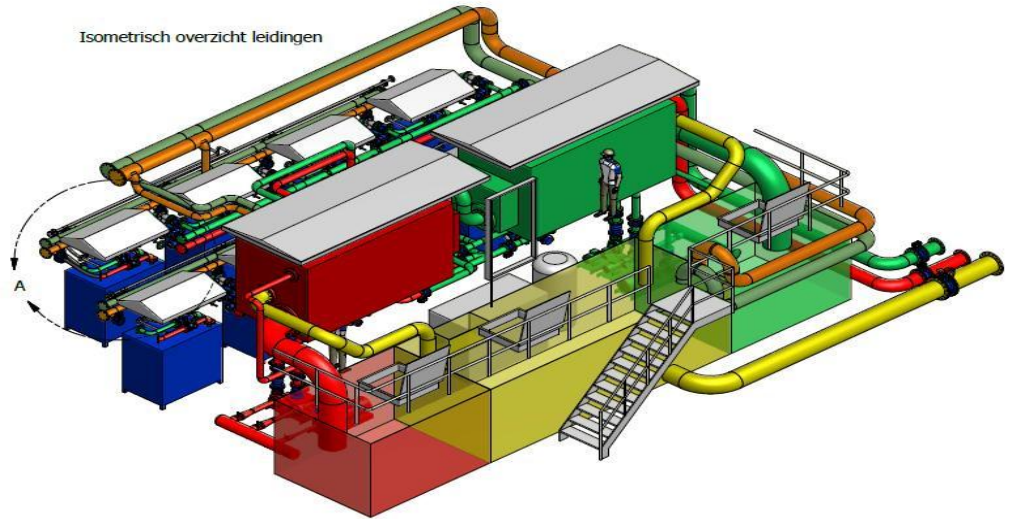
zout water aanvoer

leidingbrug

pilot installatie

zoet water aanvoer

Isometrisch overzicht leidingen



Location	: Breezanddijk
	: IJsselmeer -
	: Waddenzee
Start	: December 2011
Time frame	: 4 year
max. capacity	: 50 kW
project costs	: 7.2 million euro
subsidized	: SNN
	: province Friesland

SGP-RE: REAPower in Trapani salt pond - Sicily

Field test: 2013 -2014



Thanks for your attention !

